#### **New Solid Amine Sorbents**

- M. L. Gray<sup>1</sup>, K. J. Champagne<sup>1</sup>, Y. Soong<sup>1</sup>, J. Baltrus<sup>1</sup>,
- H. Pennline<sup>1</sup>, R. W. Stevens, Jr. <sup>2</sup>, R. Khatri<sup>2</sup>,
- S. S. C.Chang<sup>2</sup>, and S. Khan<sup>3</sup>
- <sup>1</sup>National Energy Technology Laboratory
- <sup>2</sup>Univerisity of Akron
- <sup>3</sup>Duquesne University

**Carbon Sequestration Meeting - May 2003** 



### **Overview**

#### Goals

-To develop a cost efficient process for the capture of CO<sub>2</sub>.

#### Objective

-To develop low-cost solid sorbents for the capture of CO<sub>2</sub> from flue gas streams

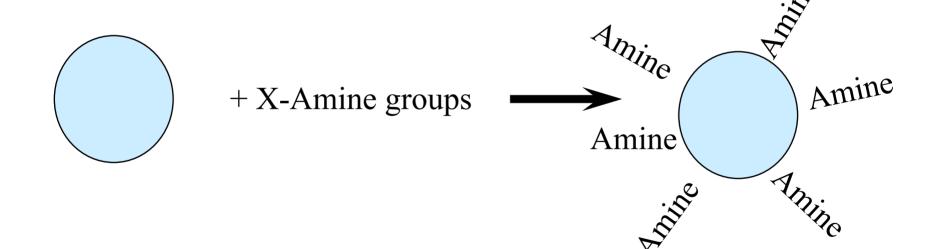
#### Technical Challenges

- To reduce the energy intensity of current capture processes (e.g., MEA process)
- -To improve the capture capacity of sorbents
- -To produce affordable solid sorbents for the capture of CO<sub>2</sub>
- -To improve the mass and heat transfer parameters
- To increase the available contact surface
- -To reduce the corrosion problems





## **Chemical Treatments**





Oxidized Surface

Amine Enriched Surface

### **Potential Applications**

- Fossil-fuel power generation plants contribute about 1/3 of anthropogenic CO<sub>2</sub> emissions
- Power generation point sources
  - Pulverized coal combustion plants
  - Advanced power system
- Capture step
  - Post-combustion
  - Pre-combustion
- Storage step in carbon sequestration requires concentrated CO<sub>2</sub>
- Natural gas clean up and Life support systems

### **Typical Chemical Stripping Process**

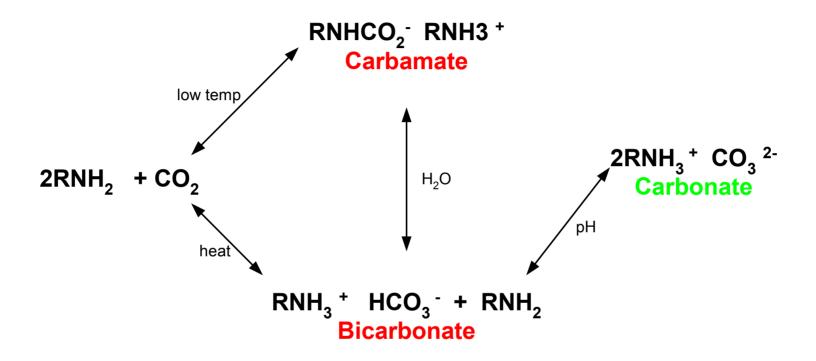
$$C_2H_4OHNH_2 + CO_2 + H_2O < Cold + H_2O < C_2H_4OHNH_3 + H_2O_3$$
Hot

Typical adsorption process is determined by the available gas/liquid interaction surface. Therefore, a large amount of liquid is needed for capture a small amount of gas.

Energy intensive

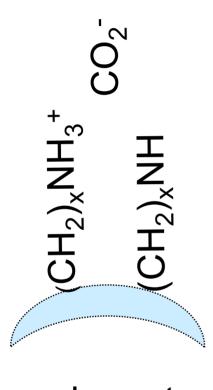


### **Proposed Reaction Sequence**

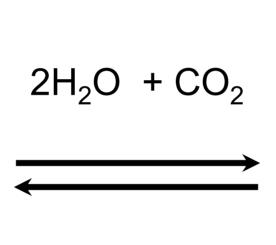


Hook, R. J., Ind. Eng. Chem. Res., 1997, 36, 1779 -1790





carbamate

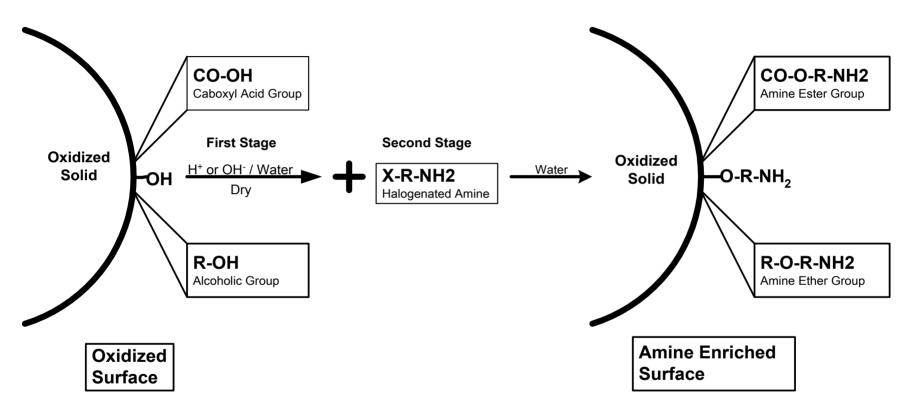


 $CH_2$ )<sub>X</sub> $NH_3$ <sup>+</sup>  $HCO_3$ <sup>-</sup>

bicarbonate

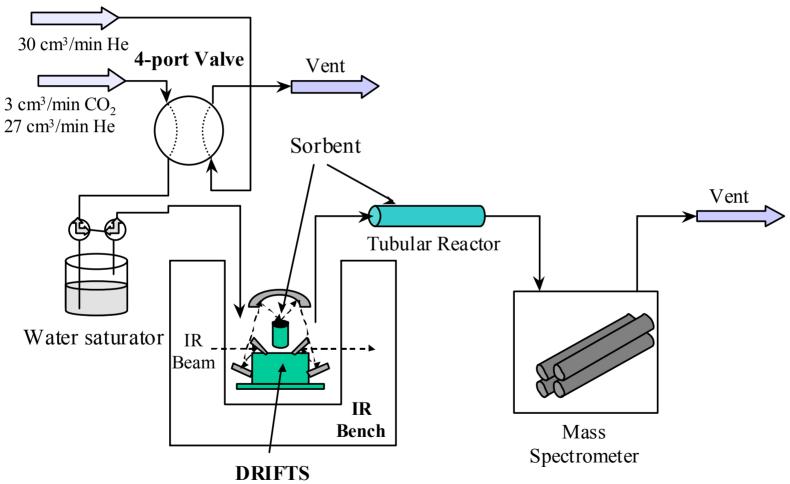


## Amine Treatment of Solid Substrates in Aqueous Media



US Patent 6,547,854 - 4/15/2003







### **Experimental TPD/FTIR Procedure**

- 15 mg in FTIR and 115 mg in TPD reactor
- Outgas in He for 4 hrs.
- Ambient T, 10 % CO<sub>2</sub> in/He
- Ambient T, switch to CO<sub>2</sub>/H<sub>2</sub>OHe
- Ambient T, switch to H<sub>2</sub>O/He to remove CO<sub>2</sub>
- TPD, 10 °C/min. to 60 or 120 °C and hold for 30 min. in He



#### **Initial Results**

- Modified fly ash derived carbon with 10<sup>-3</sup> M of 3-chloropropylamine HCL (CPAH) and 10<sup>-1</sup> M KOH
  - 95 Fly ash carbon concentrate
  - -95A CPAH and KOH
  - -95B KOH only
  - -95C CPAH only
- Tested prepared samples
  - In-situ FTIR (DRIFT) to observe the surface absorption and adsorption/desorption states
  - -TPD with on-line MS to monitor the desorbed gases



Samples Desorbed amount \( \mu mol/g \) sample

95 24

95A 81

95B 3-chloropropylamine hydrochloride

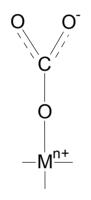
95C 174

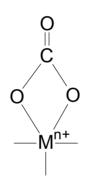
95C (regenerated) 140

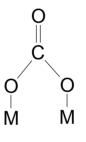


### **Proposed Species**

#### Potential Adsorption of CO<sub>2</sub> onto a Solid Surface







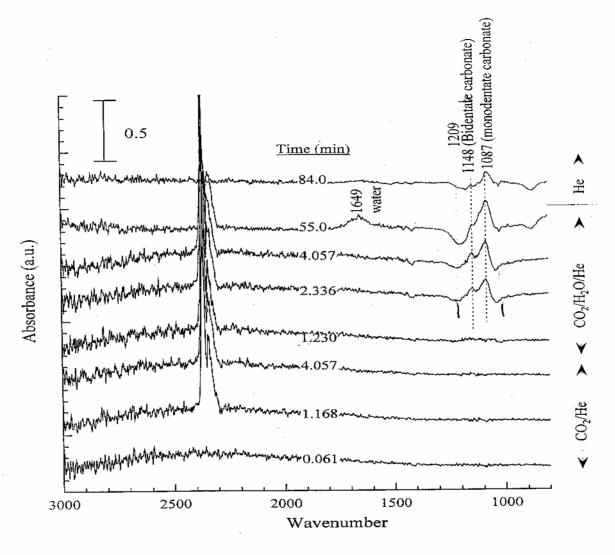
Monodentate carbonate Bidentate carbonate Bridged bidentate carbonate

$$1530 - 1470 \text{ (vas COO}^{-}\text{)} \quad 1530 - 1620 \text{ (v C=O)} \quad 1620 - 1670 \text{ (v C=O)} \\ 1300 - 1370 \text{ (vs COO}^{-}\text{)} \quad 1270 - 1250 \text{ (vas COO)} \quad 1220 - 1270 \text{ (vas COO)} \\ 1080 - 1040 \text{ (v CO)} \quad 1030 - 1020 \text{ (vs COO)} \quad 980 - 1020 \text{ (vs COO)}$$

A.C.C.Chang, et al. "In-Situ Infrared Study of CO<sub>2</sub> Adsortion on SBA-15 Grafted with

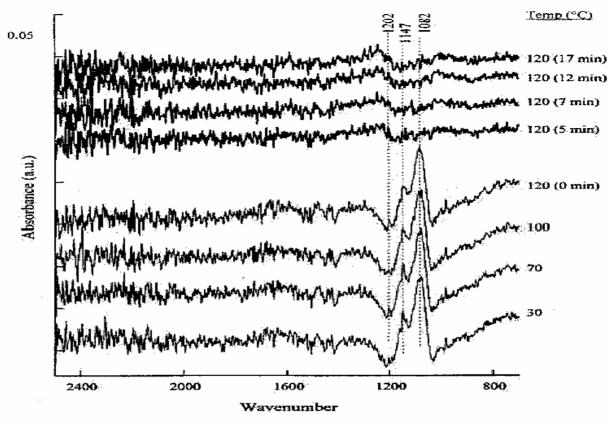
γ-Aimniopropyltriethoxy silane" Energy & Fuel, 17, pp. 468-73, 2003.





Adsorption profile of CO<sub>2</sub>/H<sub>2</sub>O over 95C





TPD profile over 95C

6/4/1.

Figure 8



## Activated Carbon Performance in CO<sub>2</sub>/He/H<sub>2</sub>O

μmol/CO2 Captured
ſ

Carbon feed 925.7

Carbon + OX 455.1

**Carbon + OX + CPAH** 1262.6

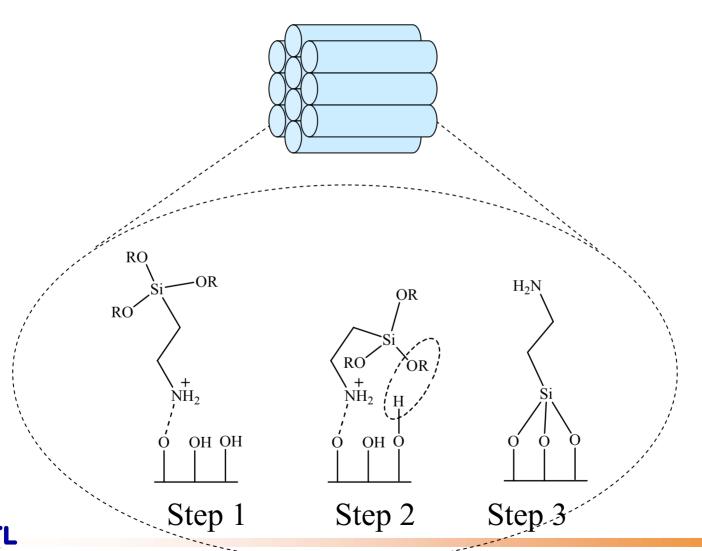
**Carbon + OX + CPAH 1021.7** 

1<sup>st</sup> Regeneration

Carbon + OX + CPAH 534.3

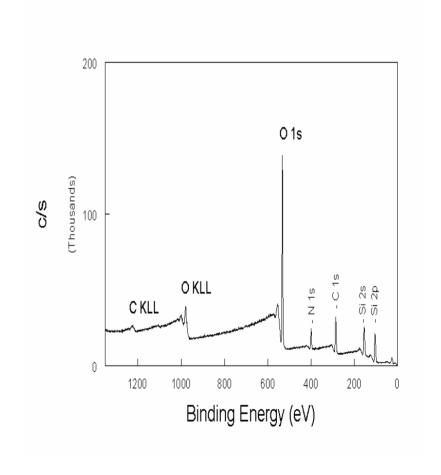
2<sup>nd</sup> Regeneration

## Preparation of the Silicon based Sorbent SBA-15 in Organic Media



## **XPS Analysis of SBA-15 Sorbent**

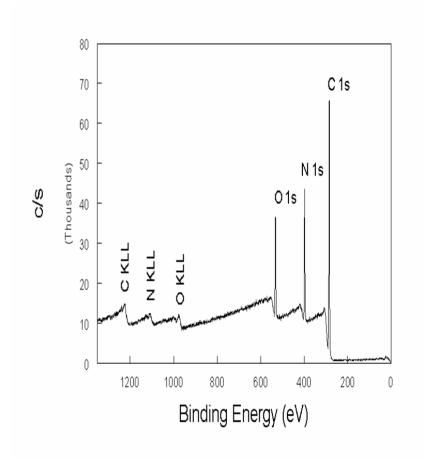
- SBA-15 Amine Sorbent.
- Nitrogen Content= 7.13%
- Surface area = 227 m2/g





## XPS Analysis of the Industrial Amine Solid Sorbent

- Industrial Amine Solid Sorbent.
- Nitrogen content= 17.73%
- Surface area = 213 m2/g





## Comparison of SBA-15 to Industrial Amine Solid Sorbent (IAS)

Sorbent	μmol/g CO <sub>2</sub> Captured	XPS % Nitrogen
SBA-15 fresh	2011.4	7.13
SBA-15 1 <sup>st</sup> regeneration	1908.5	NA
SBA –15 2 <sup>nd</sup> regeneration	1748.3	NA
IAS fresh	1603.9	17.73
IAS 1 <sup>st</sup> regeneration	1922.6	NA
IAS 2 <sup>nd</sup> regeneration	1528.1	NA

# Summary of Sorbents Performance in CO<sub>2</sub>/He/H<sub>2</sub>O

Sorbent	<b>Treatment</b>	μ <b>mol/CO</b> 2	Surface
		Captured	Area m <sup>2</sup> /g
Fly ash	Aqueous	157.2	27
Carbon	CPAH		
Carbon	Aqueous	939.5	1010
Ox + Am	CPAH		
TiO	Aqueous	1057.2	210
	Media		
SBA-15	Organic	1889.4	227
	Silicate		
IAS	<b>Immobilized</b>	1820.8	213



#### **Conclusions**

- Demonstration of the implantation of amine groups on various substrates using both aqueous and organic reaction systems.
- Aqueous 3-chloropropylamine HCL reaction system requires addition investigation to improve its performance (fly ash carbon and activated carbon).
- Organic silicate reaction system produced a sorbent (SBA-15) with similar performance to the industrial amine solid (IAS) sorbent.

